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# TU Dortmund

## Process Dynamics and Operations Group

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# Where is Dortmund?

- Dortmund is part of the Ruhr area (~ 4 million inhabitants)
  - Impressive industrial history - built upon coal and steel
  - Transformation and preservation of monuments of the past
  - It's not far to Paris, Amsterdam, Berlin...



Germany



Europe at night



Dortmund

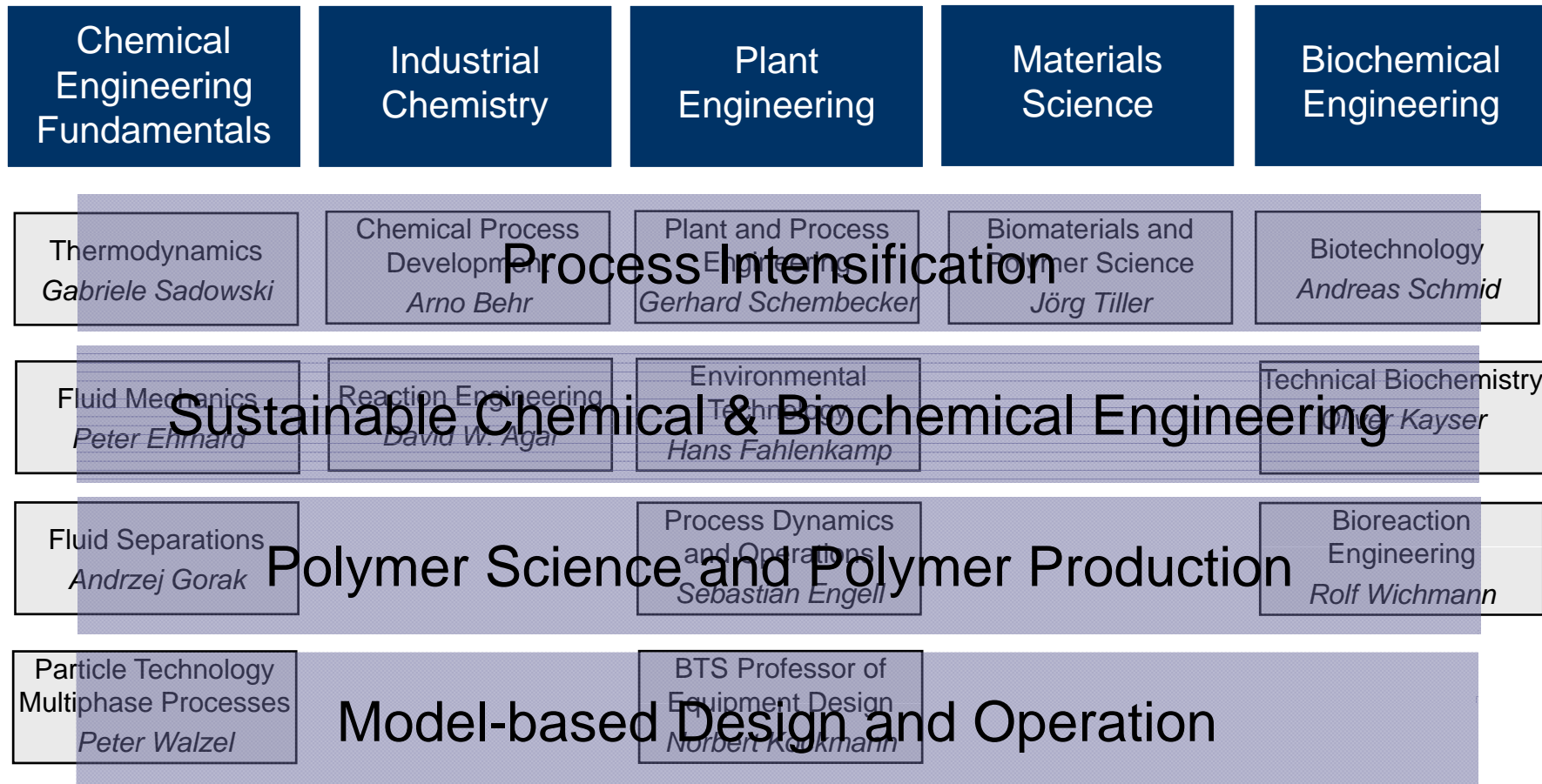
# Facts on TU Dortmund

- Dortmund is a part of the largest metropolitan area in Germany: The Ruhr
- Universität Dortmund was founded in 1968, as a step in the transition from a region of heavy industries to one of high-tec, services, and culture initially only science, engineering and business departments
- 1980 merger with a Teachers Education College (Pädagogische Hochschule Ruhr)
- 2008 renamed Technische Universität (Technical University)
- 22.000 students, 300 professors
- 16 departments, including all engineering disciplines
- Research university
- Before 2007 predominantly 4.5 year Diploma programs
- Since 2007 (forced) transition to a Bachelor/ Master system
  - 6-7 semesters for Bachelor, 3-4 for Master,  
5 years (10 semesters) overall

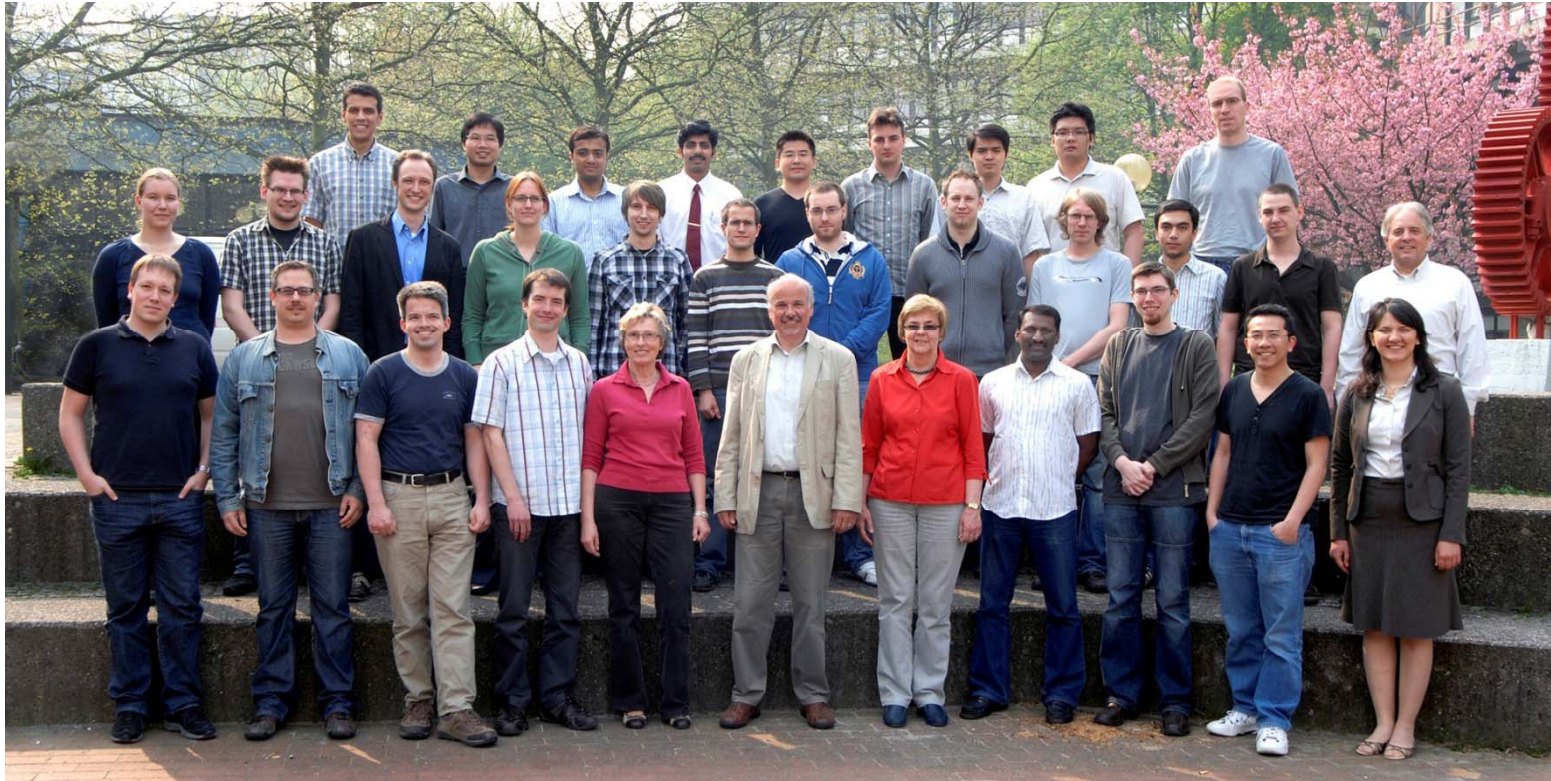
- The largest ChemE Department in Germany and among the largest in Europe
- Staff:
  - 14 Professors
  - ~ 120 doctoral students and post-docs, ~ 70 externally funded
  - ~ 20 doctoral students on scholarships
  - ~ 70 administrative and technical staff
- Programs:
  - Chemical Engineering – 140 beginners per year  
7 + 3 semesters Bachelor/Master programs
  - Biochemical Engineering – 90 beginners per year  
7 + 3 semesters Bachelor/Master programs
  - Master Program Process Systems Engineering
    - 4 semesters, 1 semester thesis work
    - Taught in English
  - Master Program Automation and Robotics/ Process Automation (interdepartmental)
- ~ 25 Dr.-Ing./ Dr. rer nat degrees granted per year

# TU Dortmund

## Biochemical and Chemical Engineering



# The DYN Team



> 20 Dr.-Ing. candidates  
3 technicians, 2 part-time secretaries  
~ 15 student assistants

# Process Dynamics and Operations

## ■ Staff

- Professor: Sebastian Engell
- ~ 20 Dr.-Ing. candidates
- 0 postdocs
- 3 technicians, 2 part-time secretaries

## ■ Teaching

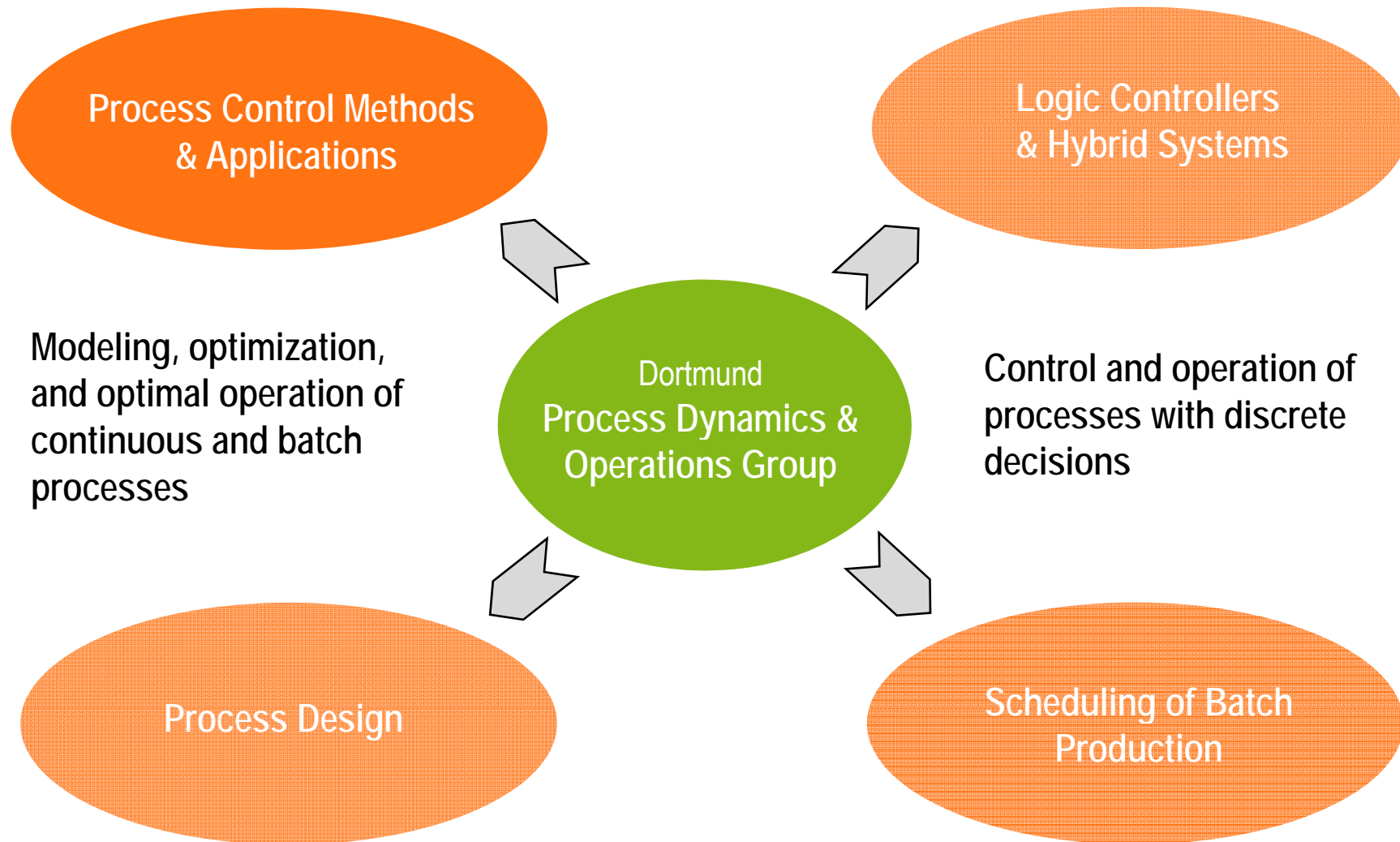
- B. Sc. Chemical Engineering / Biochemical Engineering
  - Process Dynamics and Control, Process Automation
  - Computer Programming, Control and Automation Lab
- Master PSE / ChemE
  - Advanced Dynamics and Control, Batch Process Operations
  - PSE Lab
- Master Automation and Robotics
  - Control Theory and Applications
  - Logic Control
  - Process Control Lab
  - Electives

# A&R Class of 2010





# DYN@TUDO: Areas of Research

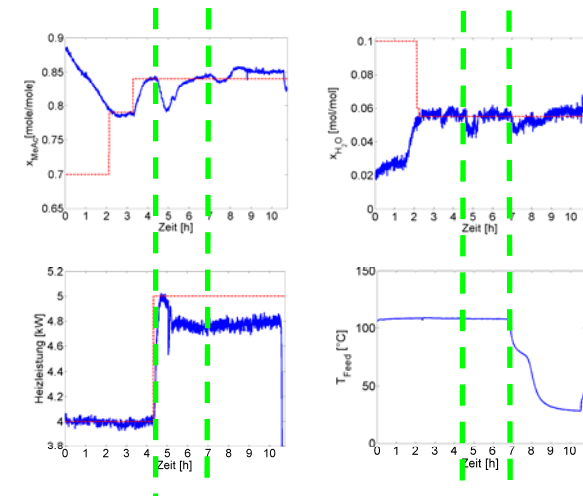
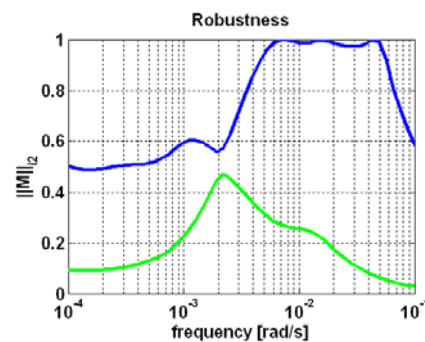


# Process Control Methods

- General approach:  
Feedback control should lead to optimal operation of a production process
- Possible realizations:
  - Optimal control structure selection
  - Optimal controller tuning



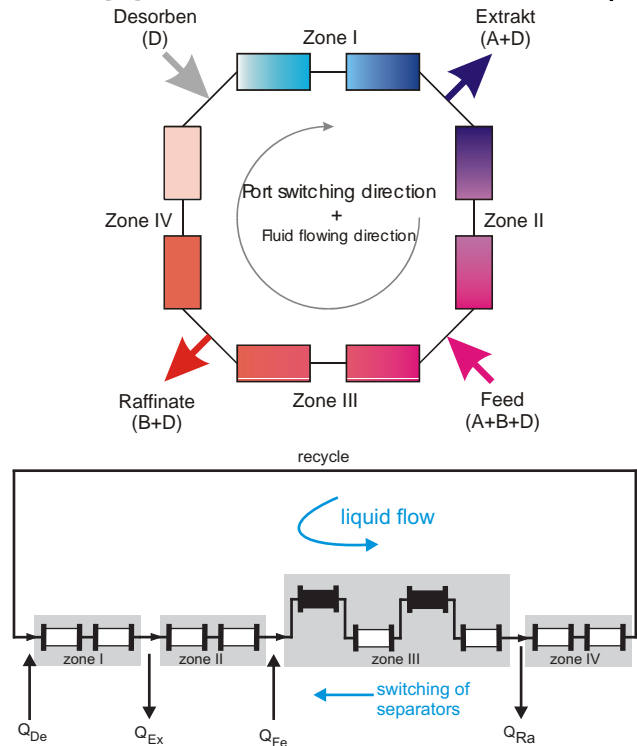
Model error modeling



- Implementation of optimal operation points by MPC (computed by RTO)
- Online optimizing control

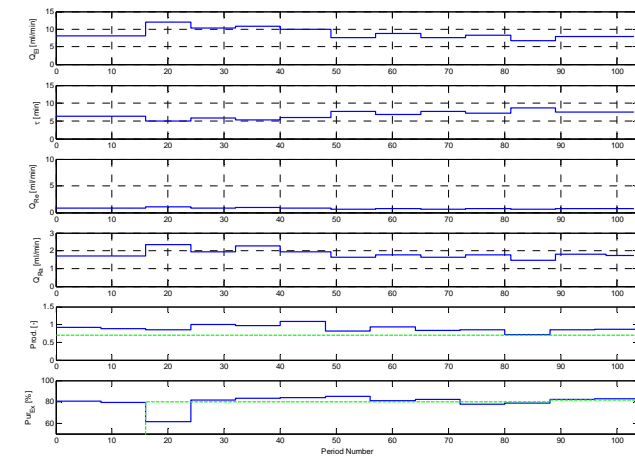
# Online Optimizing Control

- Optimize the plant performance online over a certain prediction horizon
- Implement specifications (equipment limits, purities, yield, ...) as constraints in the optimization problem – no set-point tracking
- Application: Control of (reactive) SMB processes



Novasep SMB plant, with reactors on top

Results at the real plant



## Further research:

- Moving horizon state estimation
- Handling of model errors

# Projects in Control Methods

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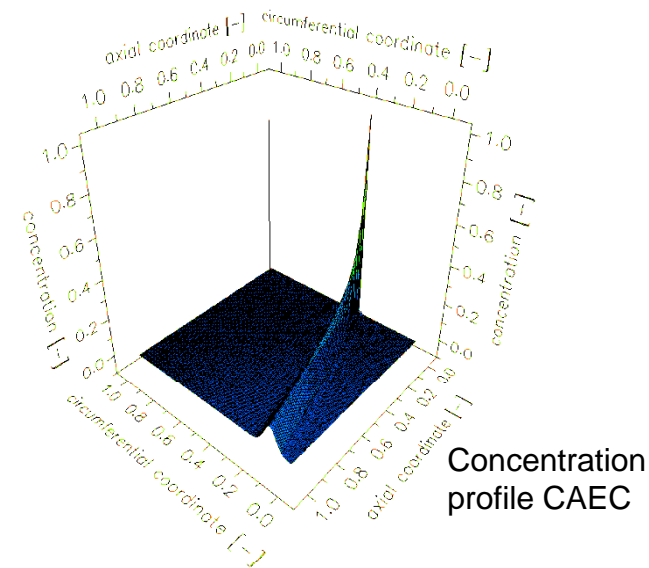
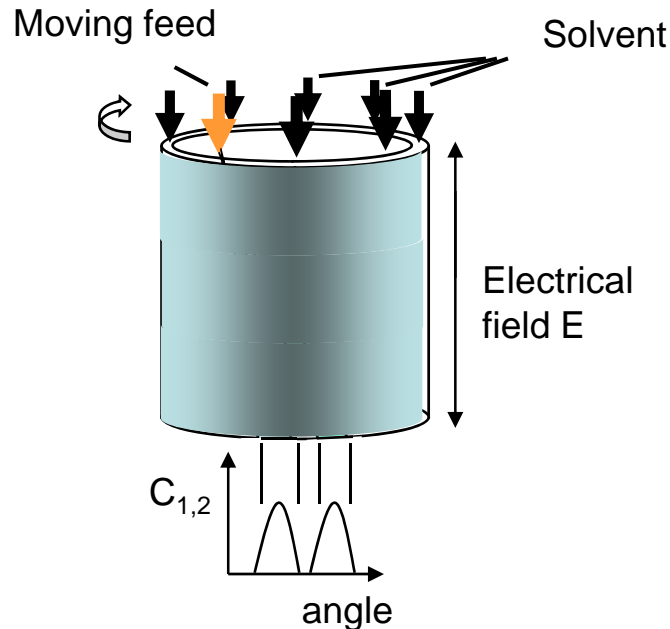
- Robust design of linear MPC controllers (Gaurang Shah)
- Selection of control structures based upon steady-state and dynamic performance (Le Chi Pham)
- Unfalsified control with controller adaptation (Ehsan Nabati)
- Robust NMPC by multi-stage optimization (Sergio Lucia, EU Project EMBOCON)
- Hierarchical control of coupled batch processes (Katja Pelz, EU NoE HYCON II)

# Applications Projects

- Dynamic modeling and control of electrochromatography (Yi Yu and Malte Behrens, EU project CAEC)
- Optimization and optimizing control of SMB processes (Malte Behrens and Roberto Lemoine, DFG)
- Modeling & control of the evolution of particle size distributions in emulsion polymerization (Ala Bouaswaig, Alireza Hosseini)
- Model-based control of complex emulsion polymerisation processes (Heiko Brandt, with BASF)
- NMPC of polymerization processes (Tiago Finkler, with Evonik)
- Continuous production of acrylic acid co-polymers (Daniel Kohlmann, EU project F3 with Rhodia and BASF)
- NMPC of reactive distillation (Elrashid Nour Eldin, funded by F3)

# Continuous Annular Electrochromatography

- Combination of Annular Chromatography and Electrochromatography



- A prototype is developed in the EU project CAEC
- Our contribution:
  - Dynamic modeling and simulation (2d pde)
  - Iterative optimizing control based upon gradient correction

# Control of Polymerisation Processes

- Control of emulsion polymerization (with BASF)
  - First principles based predictive models
  - Batch trajectory optimization
  - State estimation
  - Batch time minimization by tracking the heat removal constraint
- Particle size distribution modeling and control
  - Development of numerical methods
  - Estimation of the growth kernel
  - Experiments in 1l scale
- Control of an industrial solution polymerization (with Evonik Industries and Leikon)



Pilot Plant  
10l stainless steel reactor  
DCS controlled

Process Systems Enterprise Limited  
6th Floor East  
26-28 Hammersmith Grove  
London W6 7HA

t: +44 20 8563 0888 f: +44 20 8563 0999  
w: www.psenderprise.com



12 October 2010

**Ala Eldin Bouaswaig, Sebastian Engell**  
Process Dynamics and Operations Group  
Technische Universität Dortmund  
44221 Dortmund  
Germany

Dear Dr Bouaswaig & Prof. Engell,

**PSE Model-Based Innovation Prize winner**

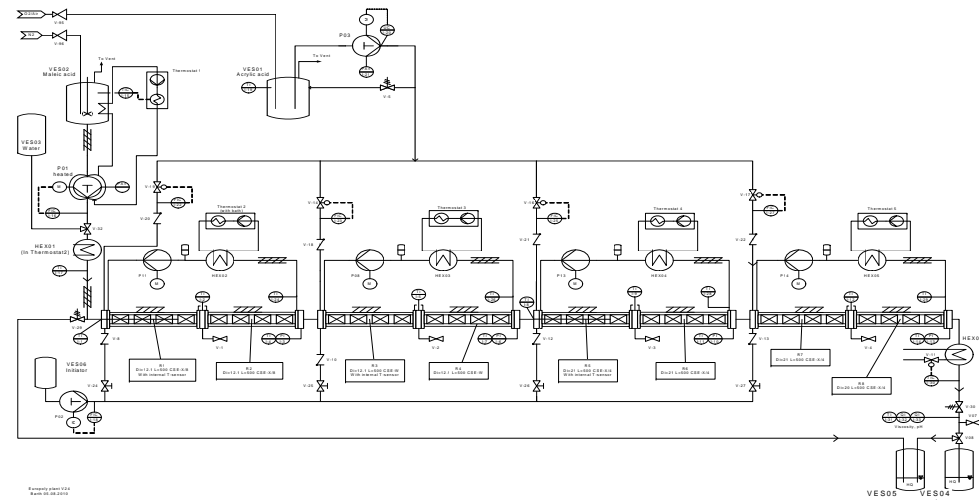
I am delighted to inform you that your paper "*WENO scheme with static grid adaptation for tracking steep moving fronts*" is the winner of the 2010 PSE Model-Based Innovation Prize.

The judges were particularly impressed by the paper, summarising it as "*an excellent technical work proposing a new numerical method for the efficient solution of parabolic differential equations, with a very nice integration with gPROMS through a foreign object*".

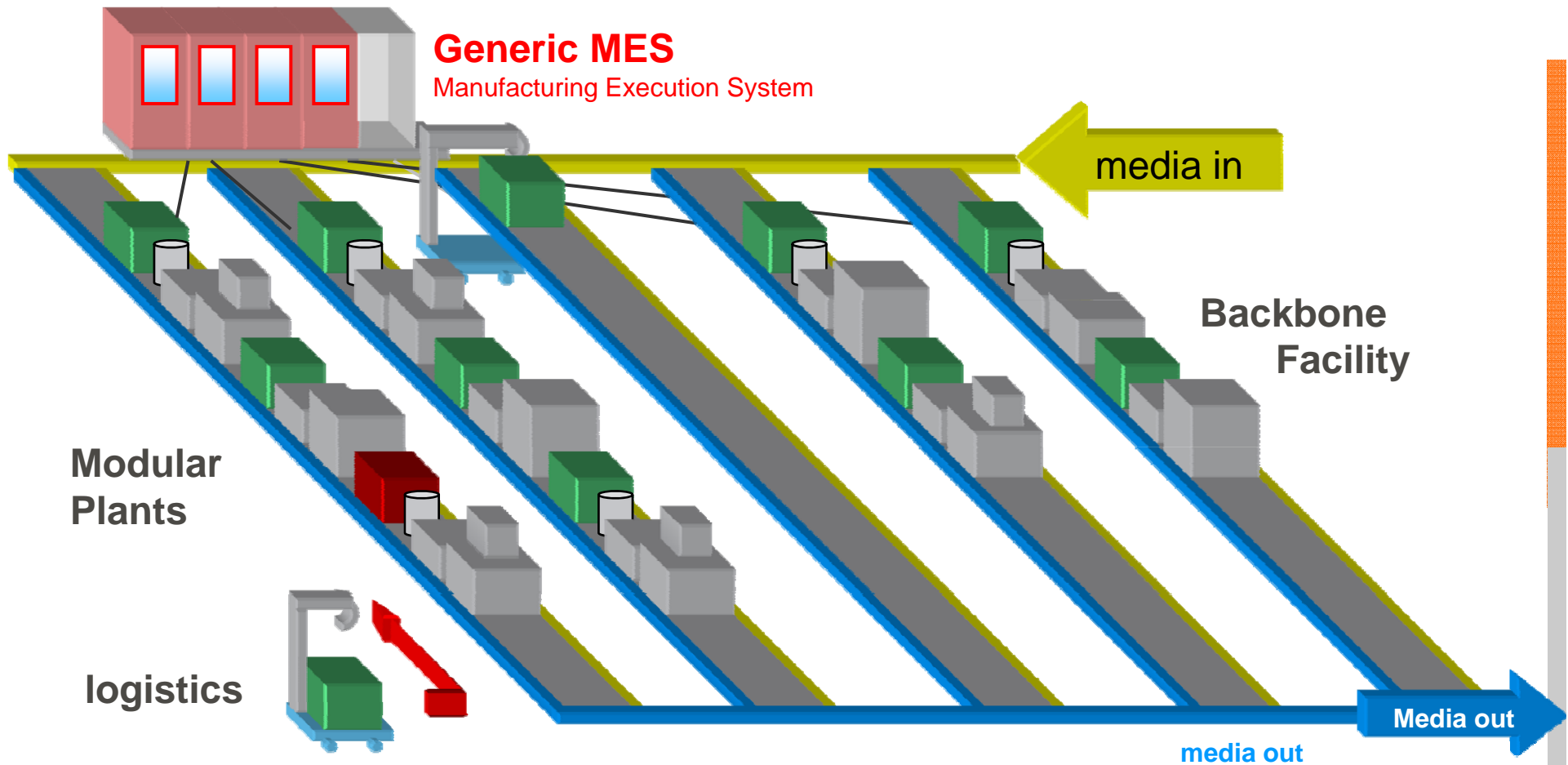


# Development and control of continuous polymerizations

- Co-polymerization of acrylic acid
- Cooperation with BASF, Rhodia in the EU Integrated Project F3



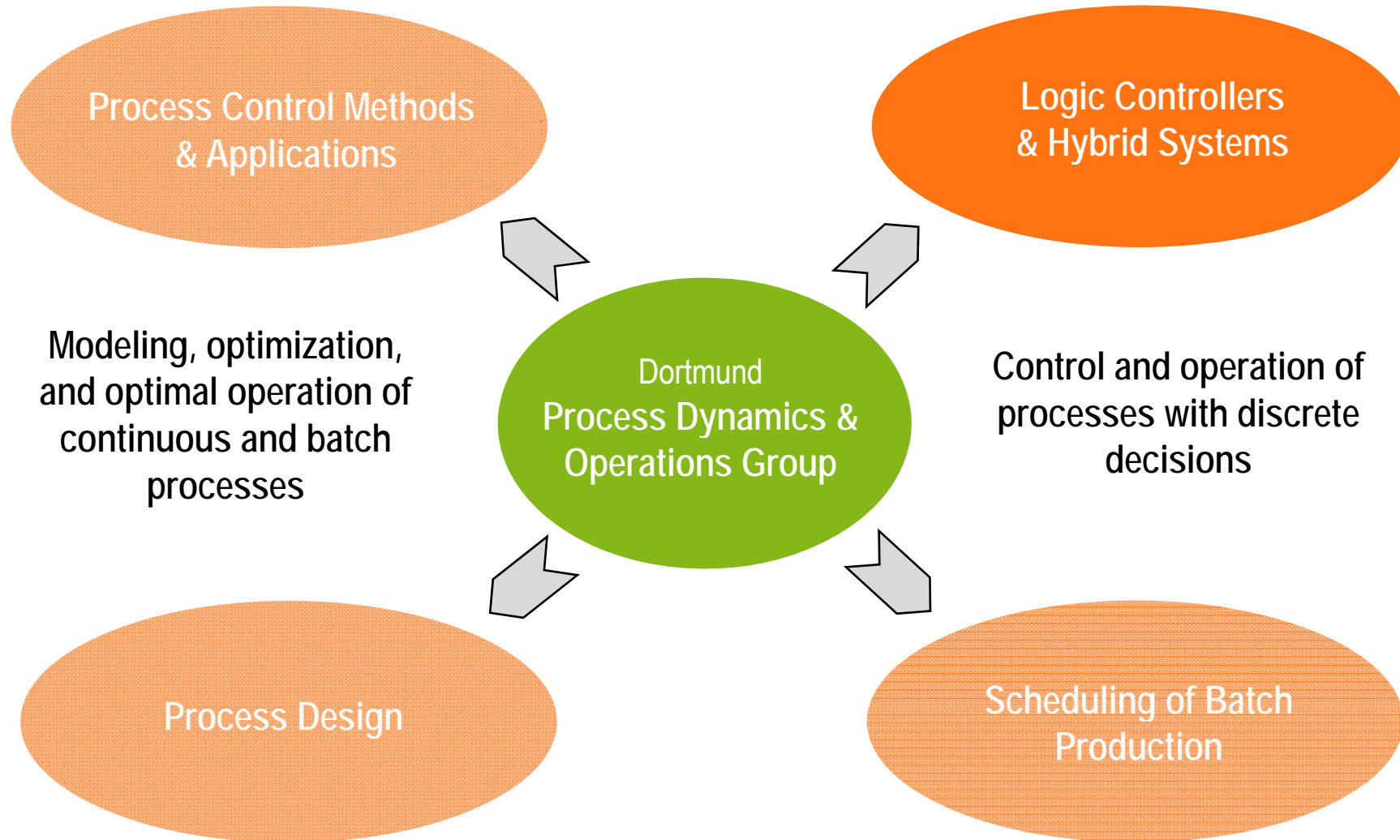
# F3-Project (Bayer, BASF, Arkema, Rhodia, Astra Zeneca, Procter & Gamble + equipment manuf. + academia)



*DYN: Lead of WP4 - Process operations*

Controllability analysis and control design for prototypical applications

# DYN@TUDO: Fields of Research

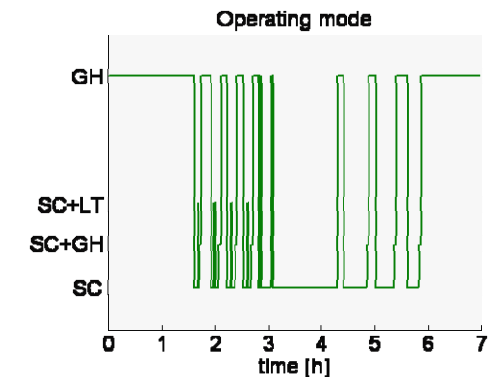
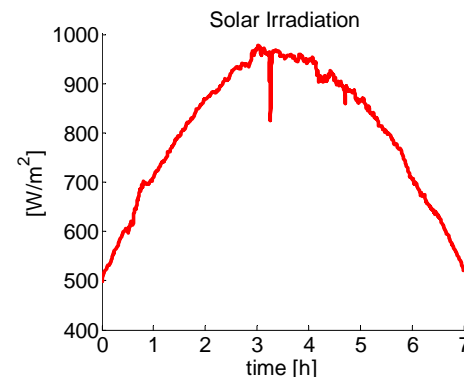
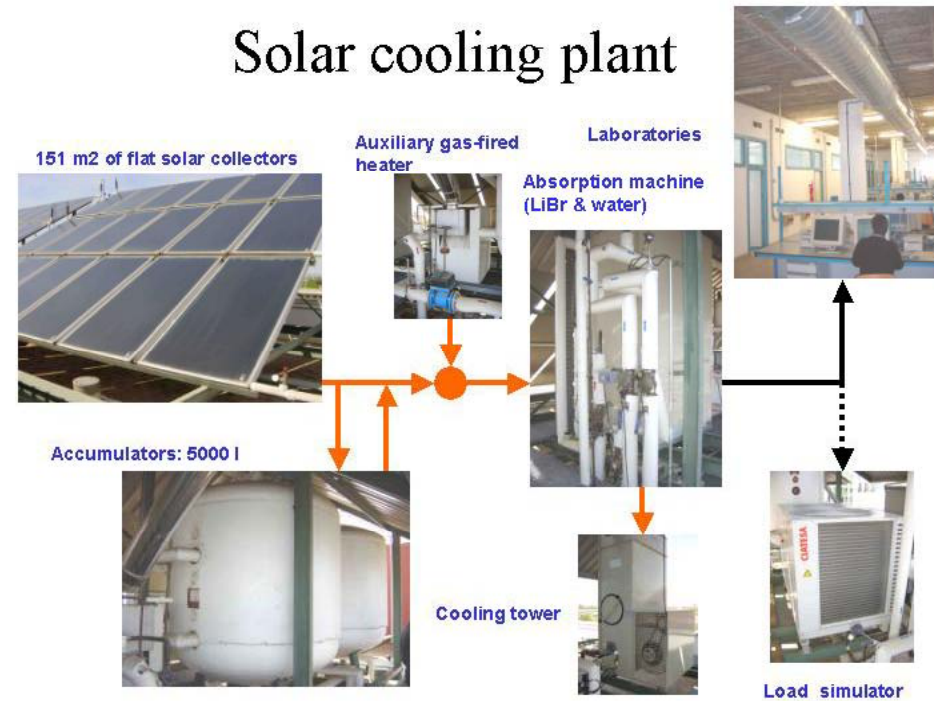


# Example of Hybrid Control Design: Control of a Solar Cooling System

Competition organized by the European Network of Excellence *HYCON*

- Plant located at the University of Seville
- Online computer control
- Remote monitoring and tuning via the internet
- Main problem: inaccurate model
- Winner: **DYN@TUDO**
- Optimizing switching strategy
- Controller provided good and robust performance in simulation and at the real plant

## Solar cooling plant



# Design and Verification of Logic Controllers

- Interaction of continuous dynamics with logic (discrete event) controllers leads to complex behavior (even chaotic behavior possible).
- Correct function is difficult to assess
- Critical logical controllers should be verified (proof of correctness), Inspection and common sense is not enough!
- Application of techniques from computer science
  - Abstraction of the continuous dynamics into (timed) discrete systems
  - Formal models of the controller and of the specifications
  - Composition and formal verification (UPPAAL, PHAVER) that controller and plant together do not violate the specifications
- ✓ Formal models of logic controllers described by SFC
- !! Abstraction of continuous models to automata models
- !! Completeness and correctness of the specification

# Current Projects in Hybrid Control

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- EU Project Multiform (Coordinated by TU Dortmund / DYN Christian Sonntag, Martin Hufner, Stephan Fischer)
  - Design support for complex controlled systems using different model formalisms and computer tools
  - Tool transformations to the Compositional Interchange Format
  - Logic controller specification and verification (DC/FT Formalism)
  - Robust verification based on approximate models
  - Systems design framework
  - Case study: Pipeless plant demonstrator
- Optimal start-up of processing plants with switching controls (NN)
- Synthesis of switching controllers (Thanh Ha Tran)

# Logic Controller Design by Refinement

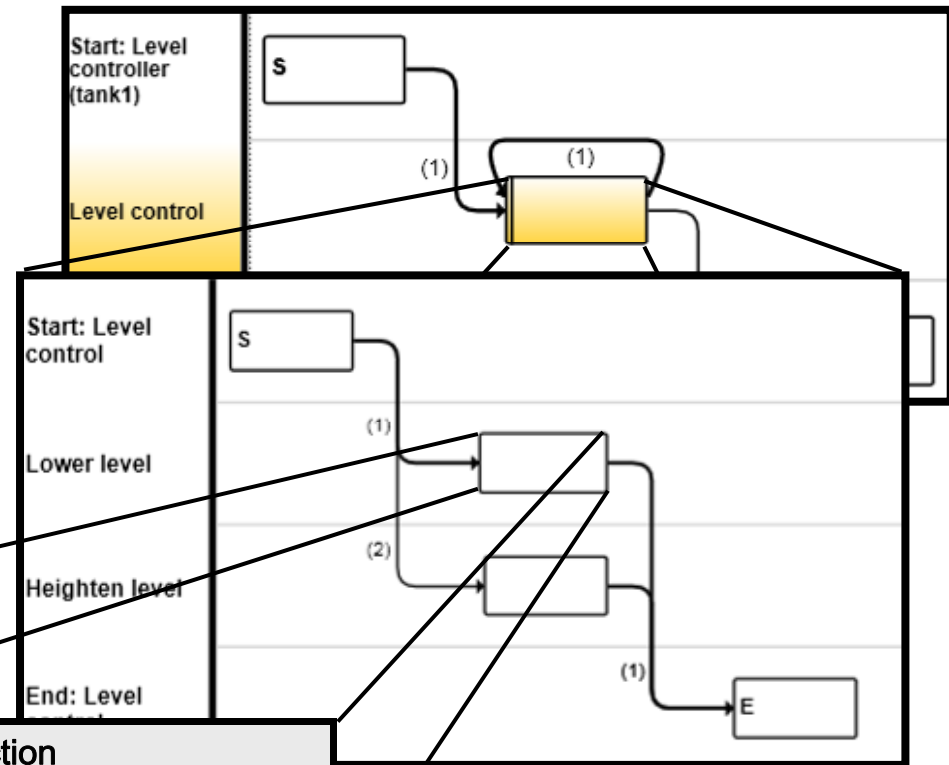
- Systematic and hierarchical approach

- Dependency Chart (DC)

- Conceptual design
    - Similar to Gantt chart
    - Hierarchy – DCs may contain DCs
    - On the lowest level, a DC is specified by a Function Table

- Function Table (FT)

- Detailed description
    - List of sequential actions
    - Documentation of design decisions

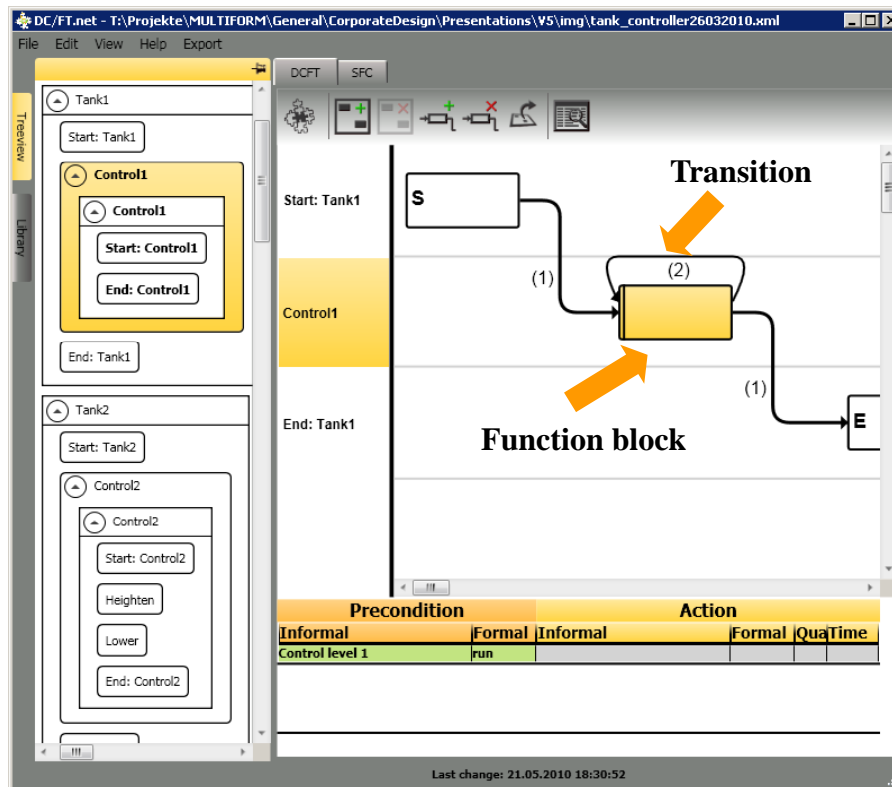


Precondition		Action		
Informal	Formal	Informal	Formal	Qualifier
<i>Tank level is to high</i>	$H > H_{max}$	<i>Open drain valve</i>	$V1 := 1$	S

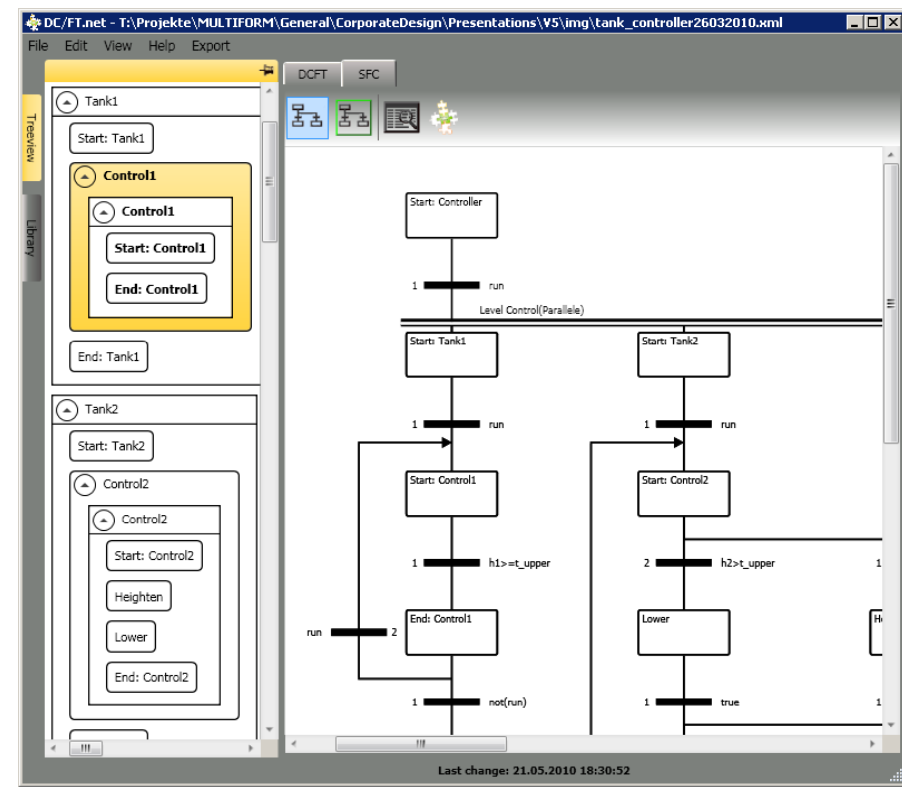
# Logic Controller Design by Refinement (2)

- Systematic refinement of informal specifications into logic controllers

DC/FT view

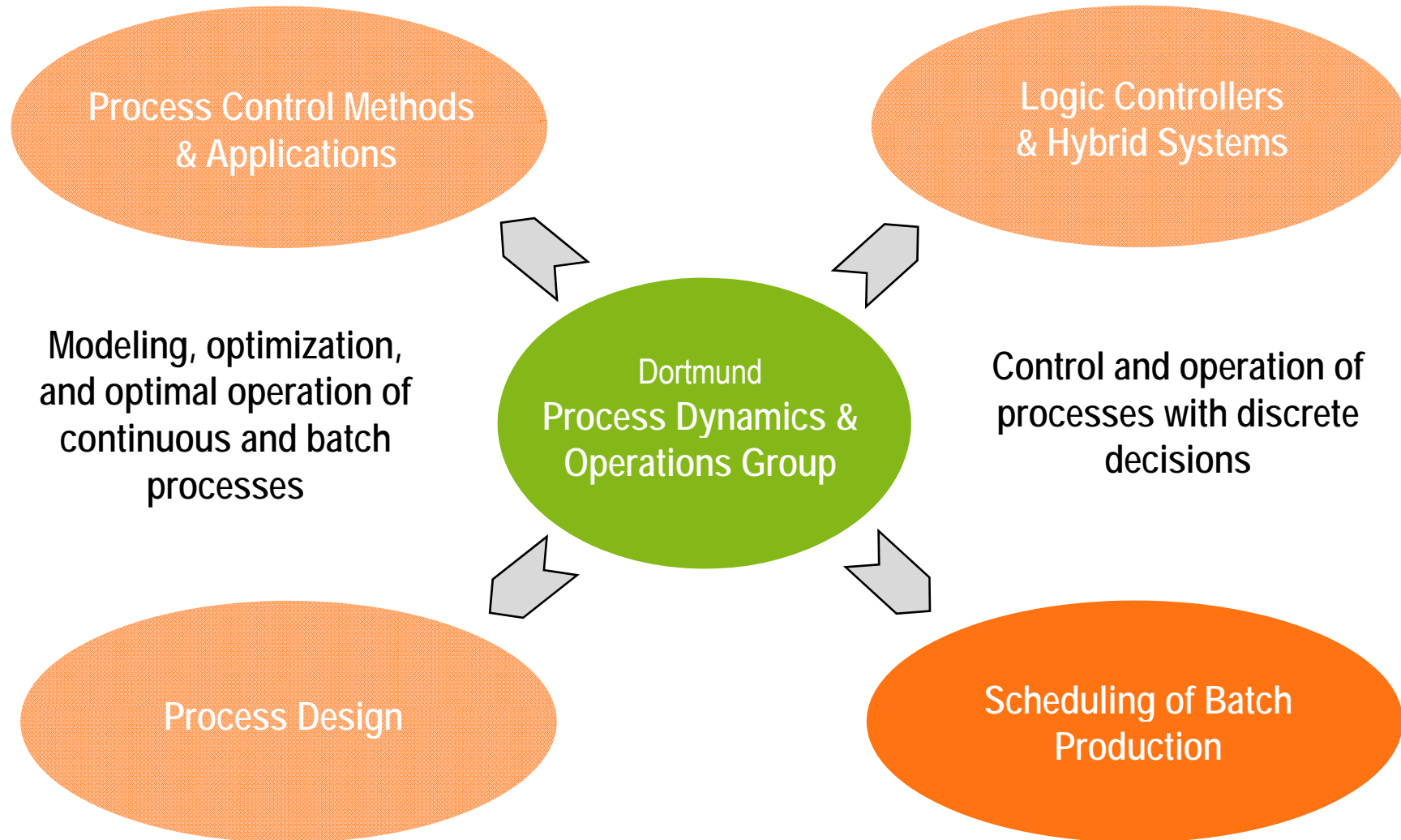


SFC view





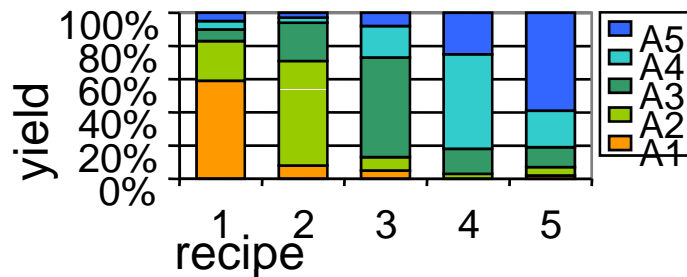
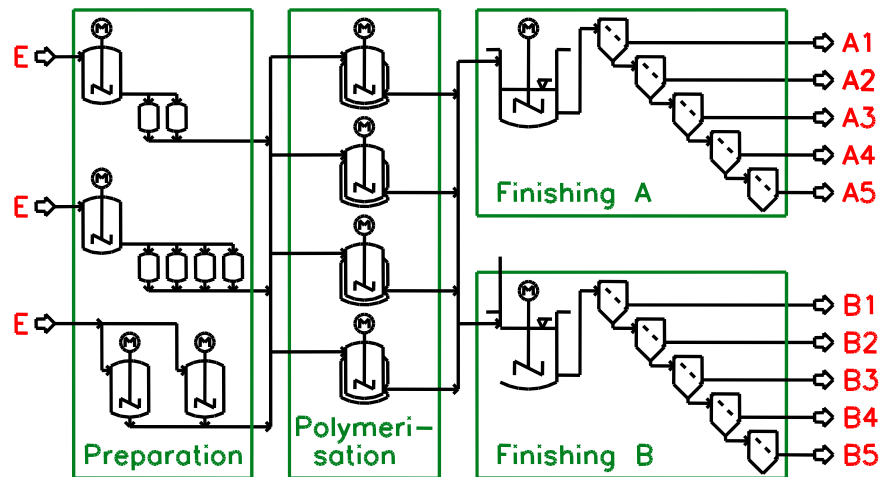
# DYN@TUDO: Fields of Research



# Production Planning and Scheduling in Batch Plants

Focus of our research:

- Online (reactive) planning and scheduling
- Dealing with uncertainties

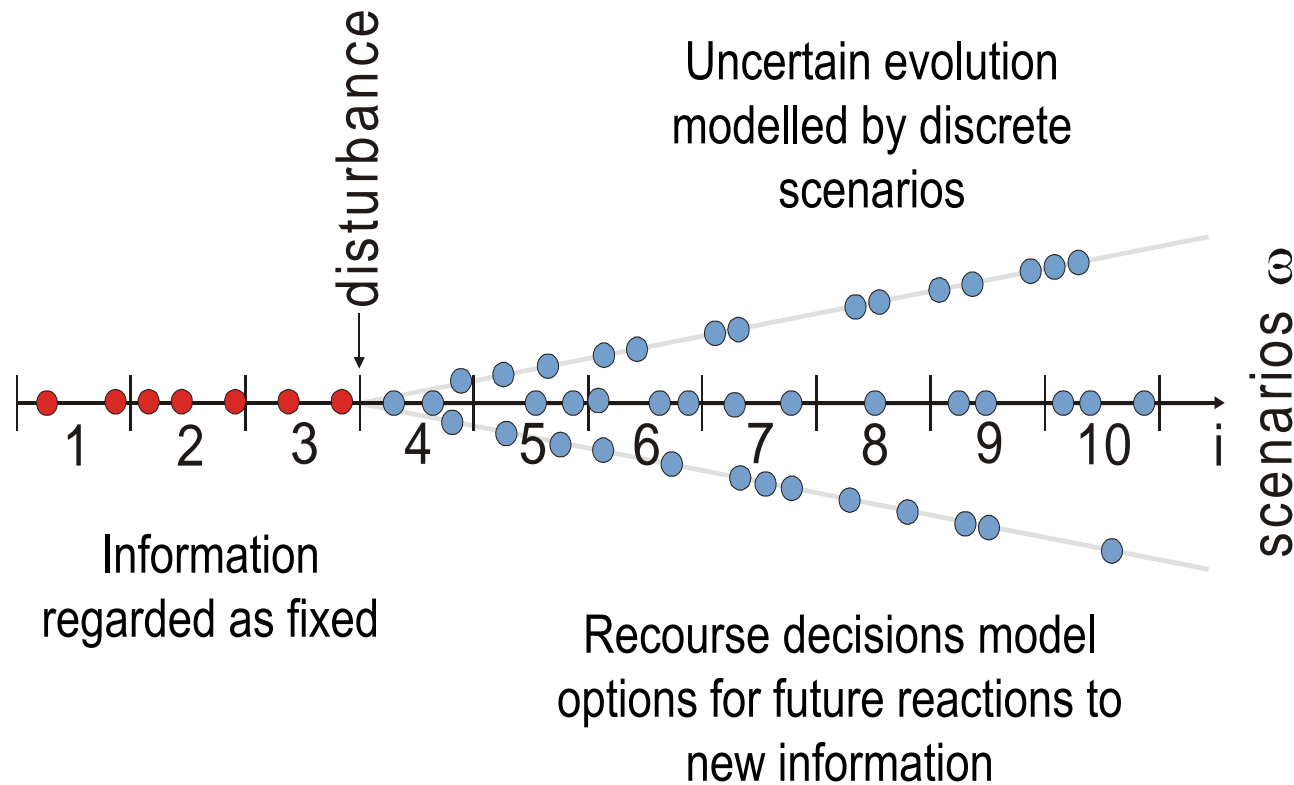


## Example EPS Process

- Decisions
  - Assignment of the recipes and timing of the batches (batching and batch scheduling)
  - Operation state finishing line
- Constraints
  - Capacity of the polymerization stage
  - Capacity of the finishing stage
  - Start-up / shut-down of the finishing stage
- Objective: maximize the profit
- Uncertainties
  - Future demands
  - Future capacity (reactor availability)
  - Yields

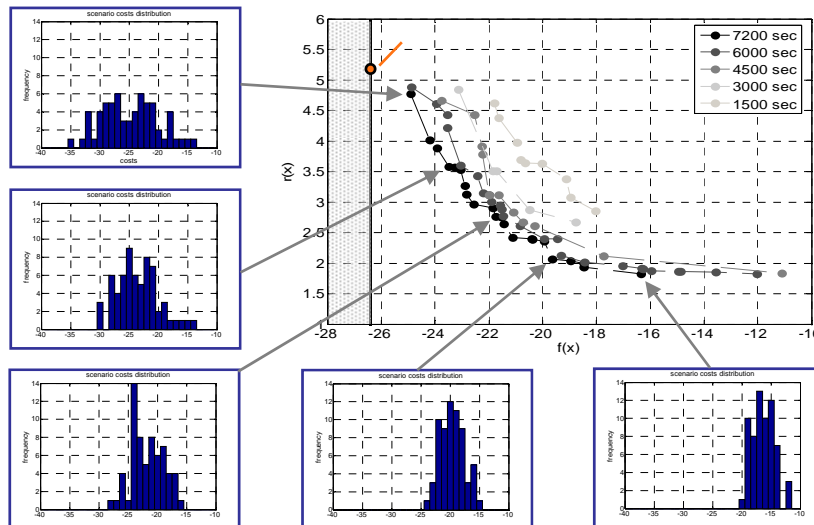
# Two-stage Decision Problem

- Information and decision-structure
  - First stage decisions  $x \neq f(\omega)$  (here and now)
  - Second stage decisions  $y = f(\omega)$  (recourse)



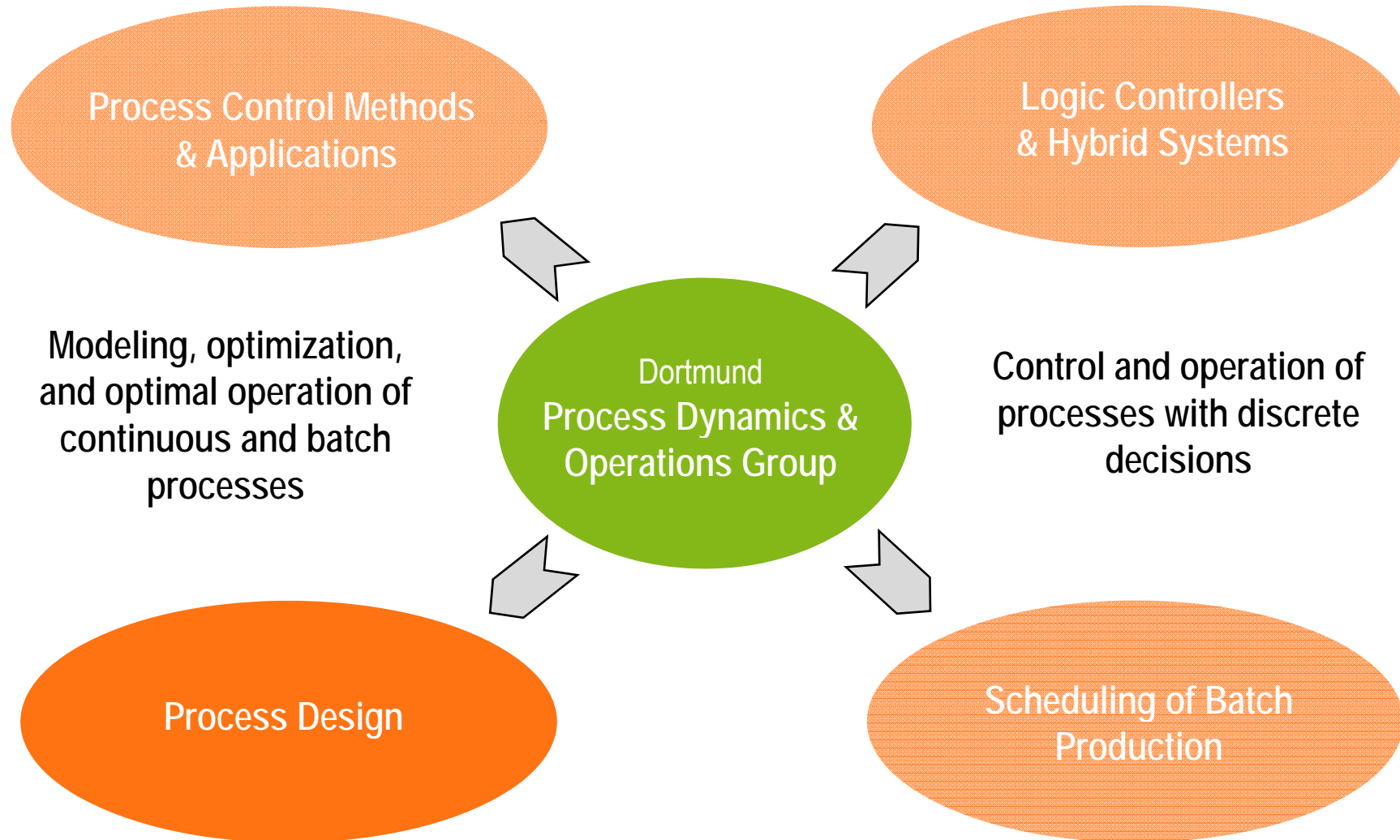
# Approaches

- Two-stage stochastic programming (Sand and Engell, C&CE 2004)
- Decomposition strategies – EA/MILP algorithms
  - Pareto front of average profit and risk (Tometzki and Engell, Comp. & Chem. Engg., in press)

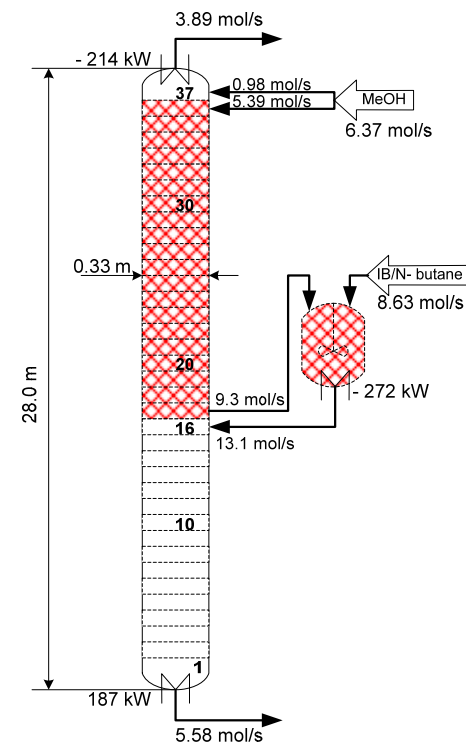
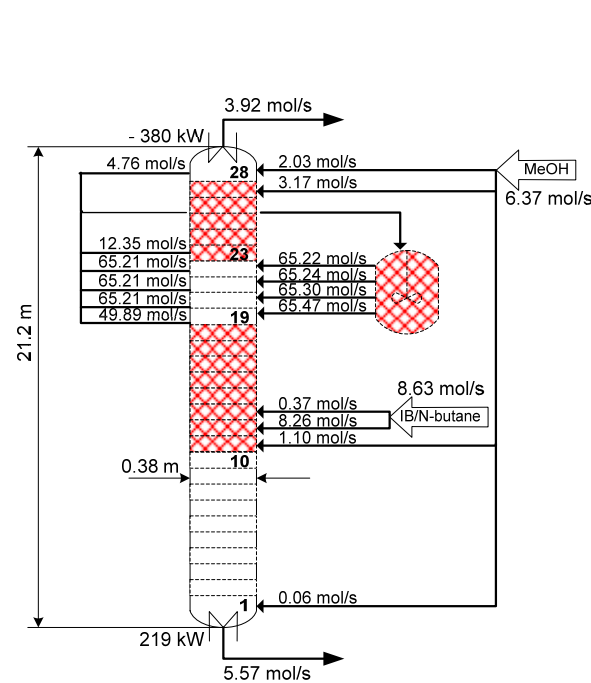


- Moving horizon scheduling based upon two-stage stochastic solution (Cui and Engell, Comp. & Chem. Engg., 2010)
- Fast scheduling using timed-automata models (Subbiah, Panek, Engell)

# DYN@TUDO: Fields of Research



# Locally Optimal Column Designs with External Reactor



- Knowledge-based initialization
- Profit:  $1,089 \cdot 10^3$  € p.a.
- Initialization by scatter search
- Profit:  $1,102 \cdot 10^3$  € p.a.

Algorithmic Challenge: Large number of local optima!

# Current Projects in Process Design

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- Memetic (EA/NLP) algorithms for complex design problems with many local optima (Maren Urselmann)
- Detection and manipulation of cycles in biological systems (Tobias Neymann/ Sven Wegerhoff)
- Model-based coordination of the development of new production processes (SFB TR 63, Jochen Steimel)